

# Dimensional Analysis

The study of the physical dimensions (force, length, time and temperature) of the variables and properties describing fluids and fluid flows.

Important uses: Consolidate data from an experiment  
Formulating empirical relations from data  
Interpreting results from model studies

## Physical Dimensions

Physical quantities have dimensions formulated in terms of four basic units:  $F$  = force,  $L$  = length,  $T$  = time, and  $\Theta$  = temperature.

Could also use the  $M, L, T, \Theta$  system where  $M$  is the mass.

Two systems are interchangeable since  $F = Ma$ .

Basic dimensions of some quantities:

velocity -  $m/s - L/T$

acceleration -  $m/s^2 - L/T^2$

mass -  $kg - M - FT^2/L$

density -  $kg/m^3 - M/L^3 - FT^2/L^4$

momentum -  $kg \cdot m/s - ML/T - FT$

stress -  $N/m^2 - F/L^2$

work -  $N \cdot m - FL$

viscosity -  $N \cdot s/m^2 - FT/L^2$

specific heat -  $cal/gr^\circ K - N \cdot m/gr^\circ K$   
-  $Fl/M\Theta - L^2/T^2\Theta$

**Dimensional homogeneity:** The terms in a relation governing a physical phenomena must have the same dimensions.

Example: Navier-Stokes equations

$$\rho \frac{Du}{Dt} = -\frac{\partial p}{\partial x} + \mu \left( \frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right)$$

$$\rho \frac{Du}{Dt} \sim \rho \frac{V}{T} \sim \frac{FT^2}{L^4} \frac{L/T}{T} \sim \frac{F}{L^3}$$

$$\frac{\partial p}{\partial x} \sim \frac{F/L^2}{L} \sim \frac{F}{L^3}$$

$$\mu \frac{\partial^2 u}{\partial x^2} \sim \mu \frac{V}{L^2} \sim \frac{FT}{L^2} \frac{L/T}{L^2} \sim \frac{F}{L^3}$$

Each term has dimensions of force per unit volume.

Dimensional Analysis and Homogeneity:

The essence of dimensional analysis is the arrangement of a collection of variables, which describe a given flow phenomena, into dimensionless groups.

Example: From Bernoulli's equation ( $p_0 = p + \rho V^2 / 2$ ),  
 $p$  and  $\rho V^2$  must have the same dimensions and, thus,

$p / \rho V^2 = (F/L^2) / (M/L^3)(L^2/T^2) = (M/LT^2) / (M/LT^2)$   
 is a dimensionless group.

Exact solution to the flow equations for a particular problem can always be arranged in terms of dimensionless groups. For the parallel plate channel

$$\dot{q} = \frac{h^3 w}{12\mu} \frac{p_1 - p_2}{L} \quad \frac{p_1 - p_2}{\rho(\dot{q}/hw)^2} = 12 \frac{L}{h} \frac{\mu}{\rho(\dot{q}/hw)h}$$

$$\dot{q}/hw = \bar{u}$$

$$\frac{p_1 - p_2}{\rho \bar{u}^2} = 12 \frac{L}{h} \frac{\mu}{\rho \bar{u} h} = \frac{L}{h} \frac{12}{\text{Re}}$$

If the solution to a given problem is not known, then we need a procedure for determining the dimensionless groups.

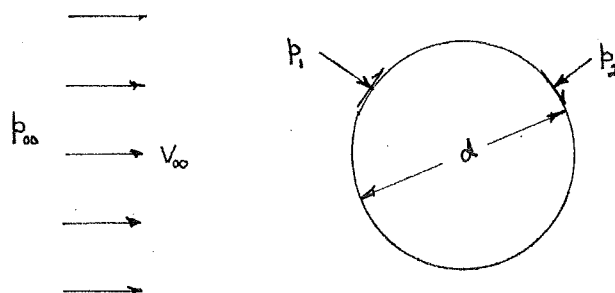
Problem: Determine a total quantity such as a resultant force, power, heat transfer, etc.

Quantity depends on other variables independent variables.

Determine these independent variables:

- 1) fluid properties ~ density, viscosity, etc.
- 2) geometry ~ length, diameter, etc.
- 3) boundary conditions ~ vehicle speed, inlet conditions

Example: Drag force on a sphere in a flow field of large extent



Flow Over a Sphere

The drag force  $F_D$  depends on the  
 density  $\rho$  (fluid property, inertia)  
 viscosity  $\mu$  (fluid property, friction)  
 diameter  $d$  (geometry)  
 velocity  $V_\infty$  (upstream condition, inertia)  
 pressure  $p_\infty$  (upstream condition, force)

$$F_D = f(\rho, \mu, d, V_\infty, p_\infty)$$

For this relation to satisfy dimensional homogeneity

$$F_D = f_1(\text{force}_1, \text{force}_2, \dots)$$

Variables  $\rho, \mu, p_\infty$  involve forces as follows:

$$\rho \sim \frac{M}{L^3} \sim \frac{FT^2}{L^4} \sim \frac{F}{V^2 d^2} \quad \text{which gives } F_\rho = \rho V^2 d^2$$

$$\mu = \frac{FT}{L^2} \sim \frac{F}{Vd} \quad \text{which gives } F_\mu = \mu Vd$$

$$p_\infty = \frac{F}{L^2} \quad \text{which gives } F_p = p_\infty L^2 = p_\infty d^2$$

Dimensionally compatible relation

$$F_D = f_1(F_\rho, F_\mu, F_p) = f_1(\rho V^2 d^2, \mu Vd, p_\infty d^2)$$

To form dimensionless groups divide by one of the force quantities =  $F_\rho = \rho V^2 d^2$  = main contributor to the drag

$$\frac{F_D}{\rho V^2 d^2} = \frac{f_1(\rho V^2 d^2, \mu Vd, p_\infty d^2)}{\rho V^2 d^2}$$

$$\frac{F_D}{\rho V^2 d^2} = f_1\left(\frac{\rho V^2 d^2}{\rho V^2 d^2}, \frac{\mu Vd}{\rho V^2 d^2}, \frac{p_\infty}{\rho V^2 d^2}\right) = f_2\left(\frac{\mu}{\rho Vd}, \frac{p_\infty}{\rho V^2}\right)$$

$$\frac{F_D}{\rho V^2 d^2} = f_3\left(\frac{1}{\text{Re}}, \frac{p_\infty}{\rho V^2}\right) = f_4\left(\text{Re}, \frac{p_\infty}{\rho V^2}\right)$$

## Drag coefficient

Dimensional analysis gives dimensionless groups

Does not give information on the functional relationship or about the physics of the flow processes.

Far field pressure  $p_\infty$  does not affect the drag force.

The drag relation

$$C_D = f(\text{Re}) \quad C_D = F_D / (\rho V^2 A / 2) = \text{drag coefficient.}$$

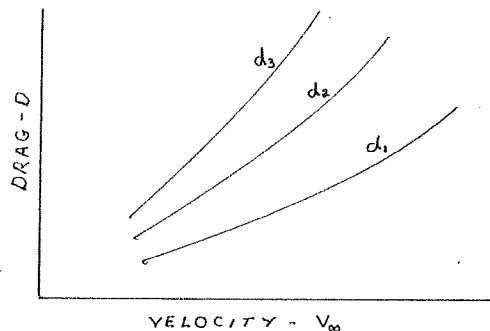
Factor of  $1/2$  is added because the dynamic pressure in Bernoulli's equation is  $1/2 \rho V^2$ .

The quantity  $d^2$  is replaced by  $A = \pi d^2 / 4$ , the projected area of the sphere.

$C_D = f(\text{Re})$  = one line on a graph

For  $F_D = f(\rho, \mu, d, V_\infty)$  there are four independent variables

Could plot  $F_D$  versus velocity  $V$  for various curves of diameter  $d$  for given values of the density  $\rho$  and viscosity  $\mu$  which would represent different fluids or even the same fluid at different temperatures.

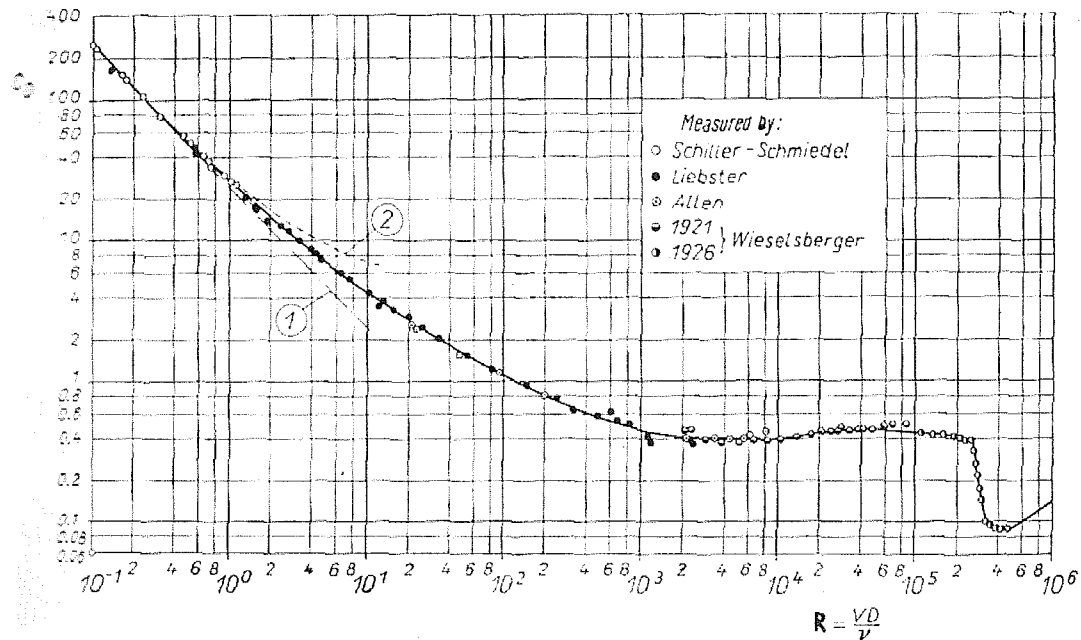


Drag on a Sphere for a Given Fluid ( $\rho, \mu$ )

Requires many pages to present the data for this relatively simple flow situation.

## Drag coefficient

Fortunately, only one curve is required with dimensionless variables for a particular geometric shape such as the sphere where  $C_D = f(\text{Re})$



Plotted with data obtained for different velocities, different diameters, and different fluids. Same curve when the drag coefficient is plotted against Reynolds number.

For instance, a 4 cm sphere moving in air at a velocity of  $V = 75 \text{ m/s}$  and in water at a speed of  $V = 5 \text{ m/s}$  have approximately the same Reynolds number of

$$\text{Re}_{\text{air}} = \frac{1.20(75)(0.04)}{1.80 \times 10^{-5}} \cong \text{Re}_{\text{water}} = \frac{998(5)(0.04)}{1.00 \times 10^{-3}} \cong 2.0 \times 10^5.$$

They both have the drag coefficient of  $C_D = 0.4$ . The drag force,  $F_D = C_D \rho V^2 A / 2$ , in each fluid is

$$\text{Air: } F_D = (0.4) \frac{1}{2} (1.2) (75)^2 (1.26 \times 10^{-3}) = 1.70 \text{ N}$$

$$\text{Water: } F_D = (0.4) \frac{1}{2} (998) (5)^2 (1.26 \times 10^{-3}) = 6.29 \text{ N}$$